

CHEMISTRY AND TRANSPORT PROPERTIES FOR JET FUEL COMBUSTION

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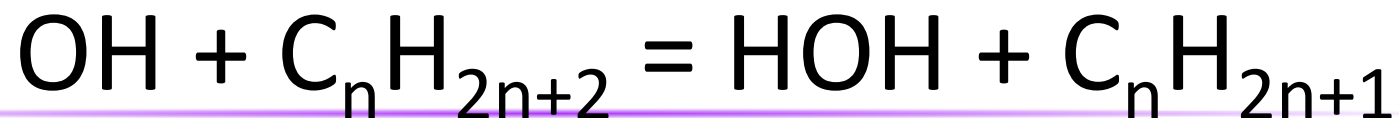


Kinetics for Jet Fuel Surrogates

- H abstraction Reaction for n-alkanes and cycloalkanes
 - Reaction Class approach to calculate rates
- The RC-TST
 - supports the assignment of equal rates for reaction in the same class through the use of the Evans/Polanyi relationship and RC-TST parameters
 - Helps to define uncertainties in the mechanism

Reaction Class Transition State Theory

- RC-TST: reactions in a given class – same reactive moiety – have similar potential energy surfaces along the reaction coordinate.
- LER: Within a class there is a linear relationship between barrier heights and reaction energies.



- Primary Carbon
 - $\text{OH} + \text{CH}_3\text{CH}_3 = \text{H}_2\text{O} + \text{CH}_2\text{CH}_3$
- Secondary Carbon
 - $\text{OH} + \text{CH}_3\text{CH}_2\text{CH}_3 = \text{H}_2\text{O} + \text{CH}_3\text{CHCH}_3$
- Tertiary Carbon
 - $\text{OH} + (\text{CH}_3)_2\text{CHCH}_3 = \text{H}_2\text{O} + (\text{CH}_3)_3\text{C}$

Reaction Class Transition State Theory

$$k_a(T) = f_\kappa(T) f_\sigma(T) f_Q(T) f_V(T) k_p(T)$$

$k_p(T)$ (Reference Reaction)

$$f_\kappa(T) \text{ (Tunneling Factor)} = \frac{\kappa_a}{\kappa_p}$$

$$f_\sigma(T) \text{ (Symmetry Number Factor)} = \frac{\sigma_a}{\sigma_p}$$

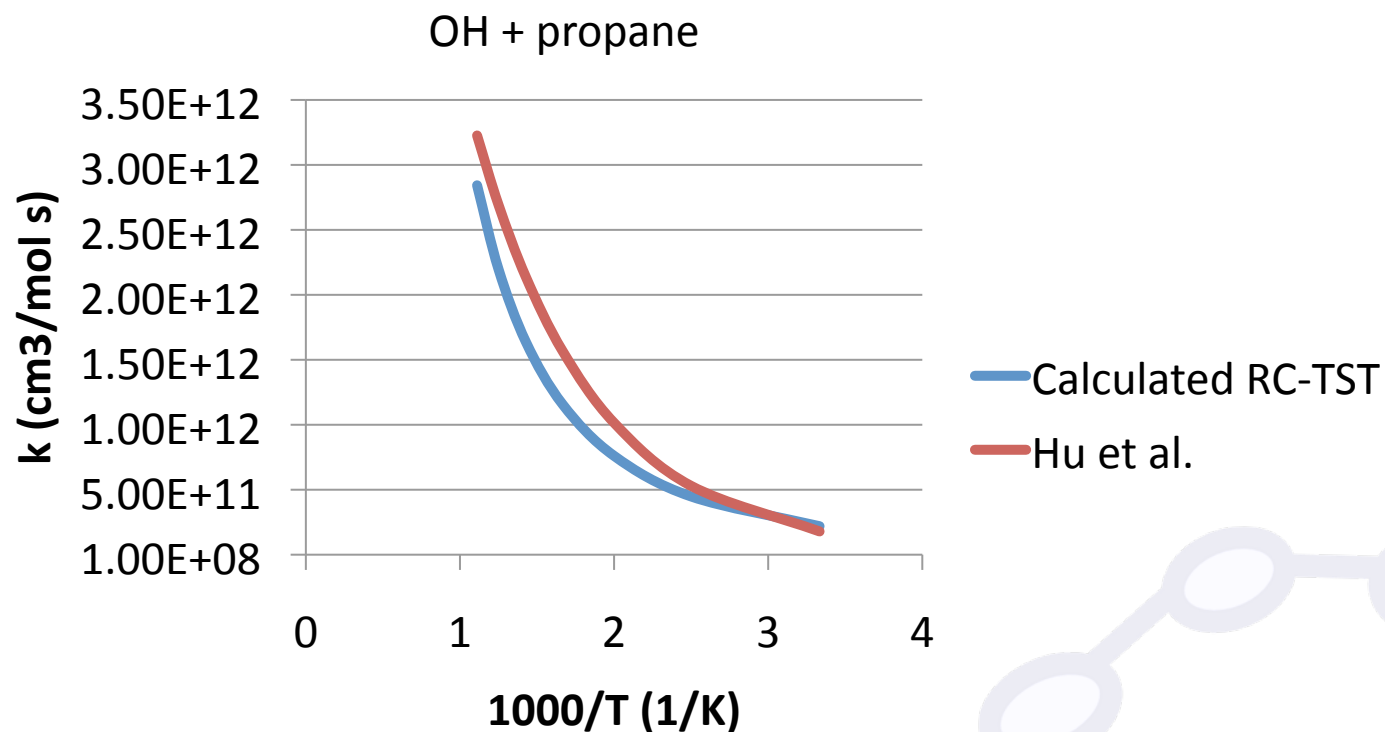
$$f_Q(T) \text{ (Partition Function Factor)} = \frac{\frac{Q_a^\ddagger(T)}{Q_p^\ddagger(T)}}{\frac{\Phi_a^\ddagger(T)}{\Phi_p^\ddagger(T)}}$$

$$f_V(T) \text{ (Potential Energy Factor)} = \exp\left(-\frac{\Delta V_p^\ddagger - \Delta V_a^\ddagger}{R_u T}\right)$$

ΔV^\ddagger : Barrier Height

Truong et al. 2006

Comparison to Known Rates



W. P. Hu, I. Rossi, J. C. Corchado and D. G. Truhlar, "Molecular modeling of combustion kinetics. The abstraction of primary and secondary hydrogens by hydroxyl radical," *J Phys Chem A*, vol. 101, pp. 6911-6921, 1997.

Transport Properties

- Modeling practical fluid systems requires the knowledge of mass diffusion coefficients over wide range of temperatures and pressures.
- The strong coupling of heat conduction and molecular diffusion in reacting flows demands an accurate description of the mass diffusivities of various species for flame structure simulations.

Small variation of fuel diffusivity should be considered to explain flame characteristics accurately

Critical role of mass diffusivity in Combustion

Ignition characteristics of n-heptane diffusion flame

Andac and Egolfopoulos, 31th Int. Sym. Combust. 2007

- 10% perturbation of n-C₇H₁₆ diffusivity
→ 50K change of ignition temperature – influence rates

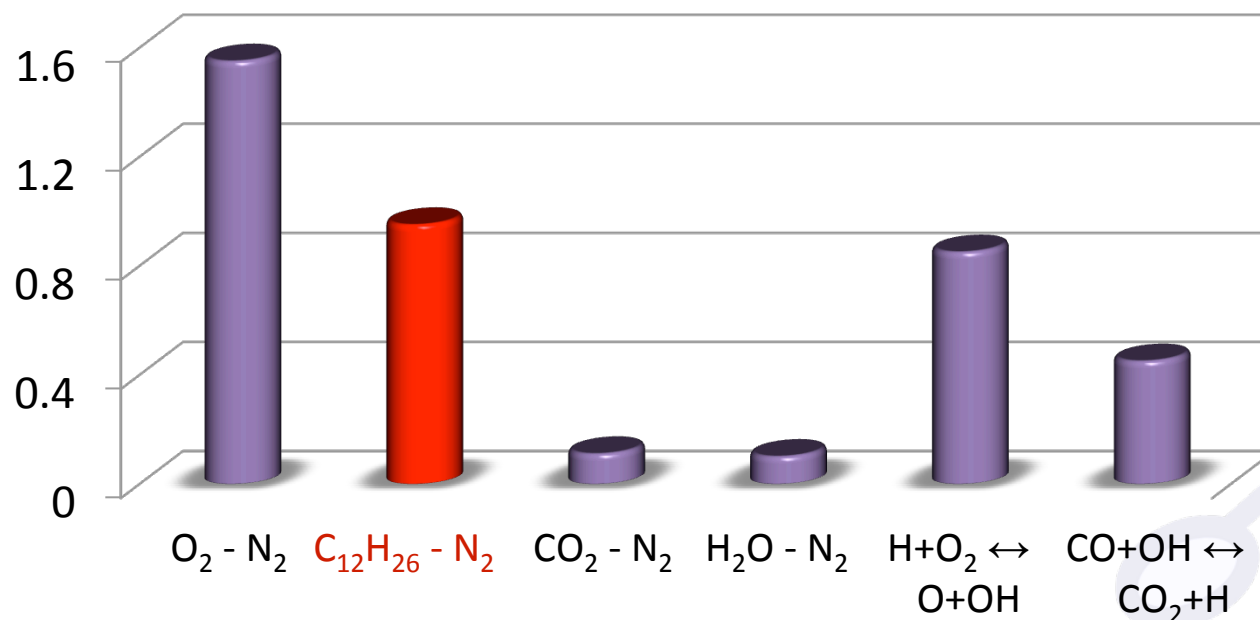
Extinction characteristics of methane/air flame

Dong et al.. 2005

- Use different transport models
→ 20 ~ 40% discrepancies in flame properties

Critical role of mass diffusivity in Combustion

Logarithmic Sensitivity to extinction strain rate



Air- $C_{12}H_{26}$

Diffusion flame

403K, 1 atm

Fuel/ N_2 mass

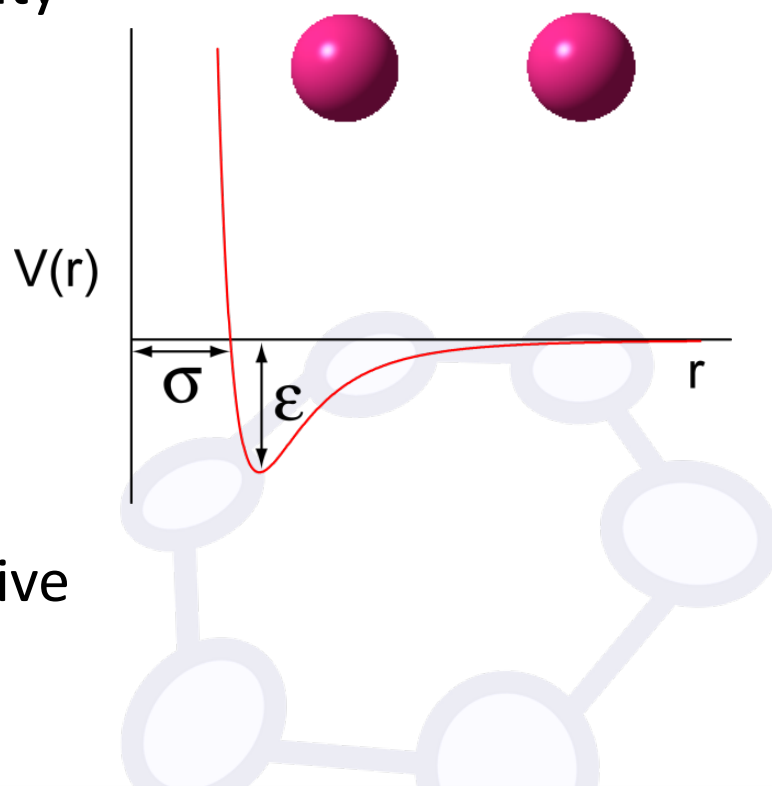
ratio = 0.05 ~ 1

[Holley, You,
Dames, Wang,
Egolfopoulos, 32th
Int. Sym.
Combust., 2008]

non-premixed counterflow flames: Amount of fuel accessible is diffusion controlled

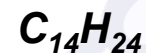
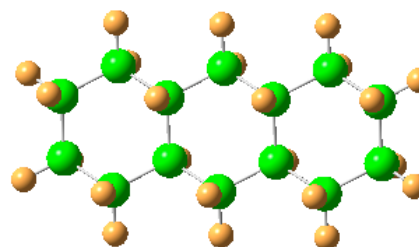
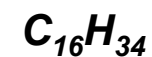
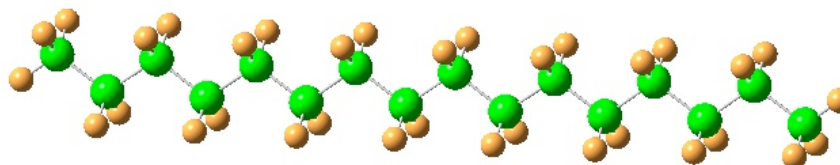
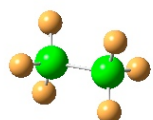
Limitations/Assumptions of this approach

- Diffusion function of tabulated collision integrals, mainly derived from viscosity measurements
- Binary collision – dilute systems
- Spherical potential – averaged over orientations of the molecules
- Potential parameters
- High temperature conditions – uncertainties especially in the repulsive part of the potential



Spherical potential

- How good is this approach for molecules that have non-spherical structure



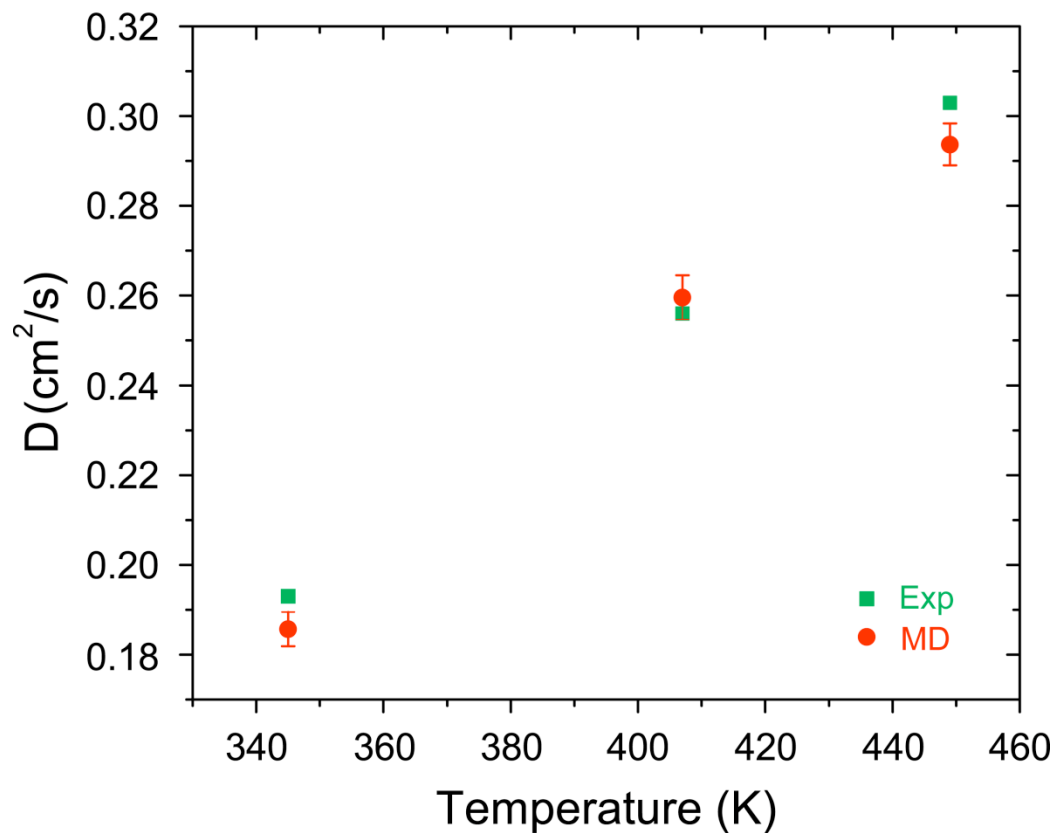
Objectives

- ❑ Implement a computational tool to determine the binary mass diffusion coefficients of hydrocarbon from **fully atomistic Molecular Dynamics simulations**
- ❑ Identify the effect of molecular structure on diffusivity
Possible factors that can be used to take into account morphology
- ❑ The validated computational tool can be used to gain insights on the transport properties of various systems at different temperatures where experimental data are not available

Computational approach

1. Fully atomistic force field parameters (OPLS-AA)
2. Canonical ensemble (NVT ensemble)
: remove the pressure coupling effects
3. Systems of ~7000 molecules, 500 – 1000K, 1 atm
5. 1.0 fs time step for numerical integration
7. 7 ns relaxation time for the integral of correlation functions

Benchmark of the computational approach



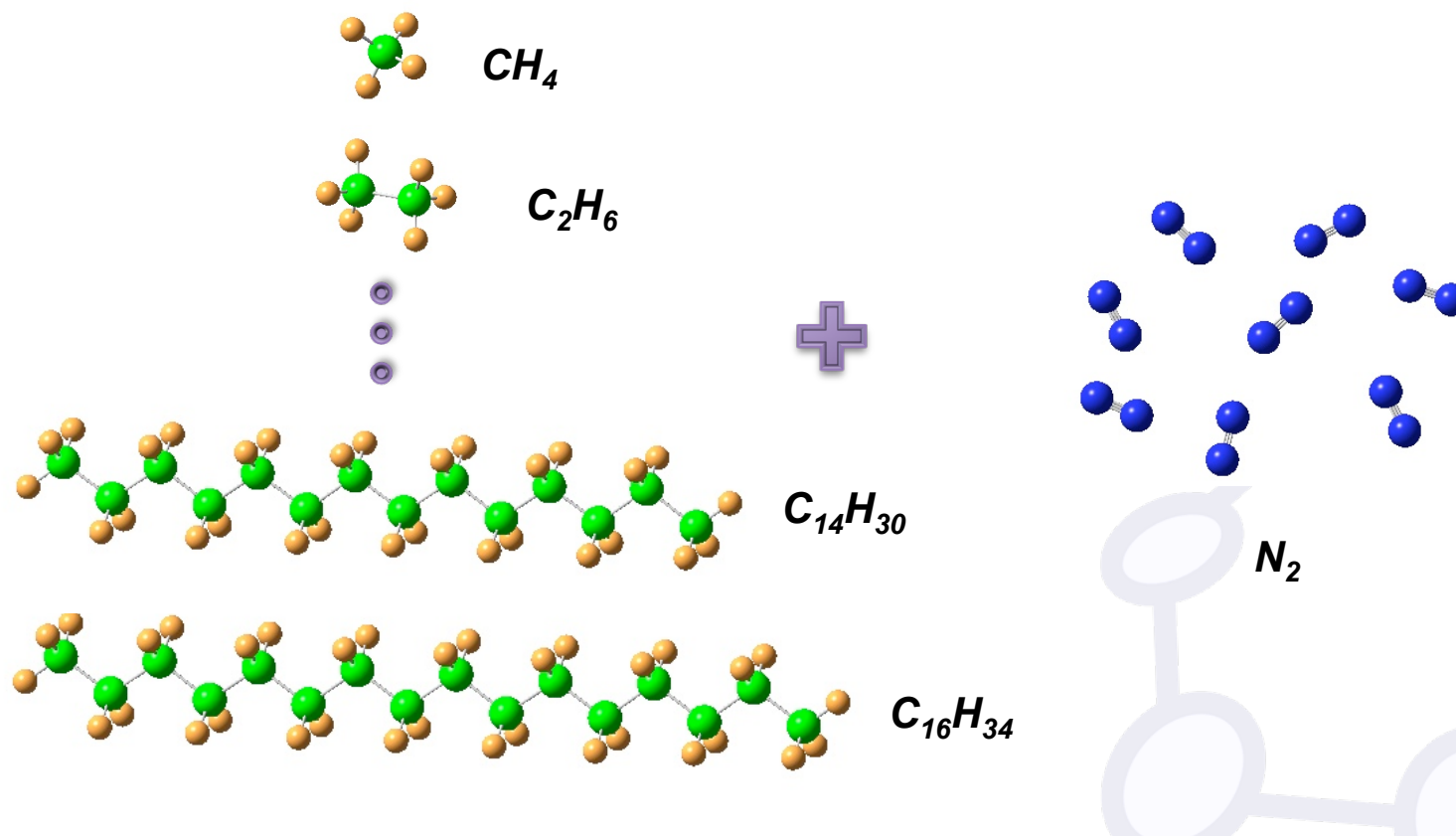
		D_{12} [cm ² /s]	
Mixture	T [K]	Exp	MD
C ₂ H ₆ /N ₂	345	0.193	0.186
	407	0.256	0.259
	449	0.303	0.294
C ₅ H ₁₂ /N ₂	353	0.136	0.121

[Exp:

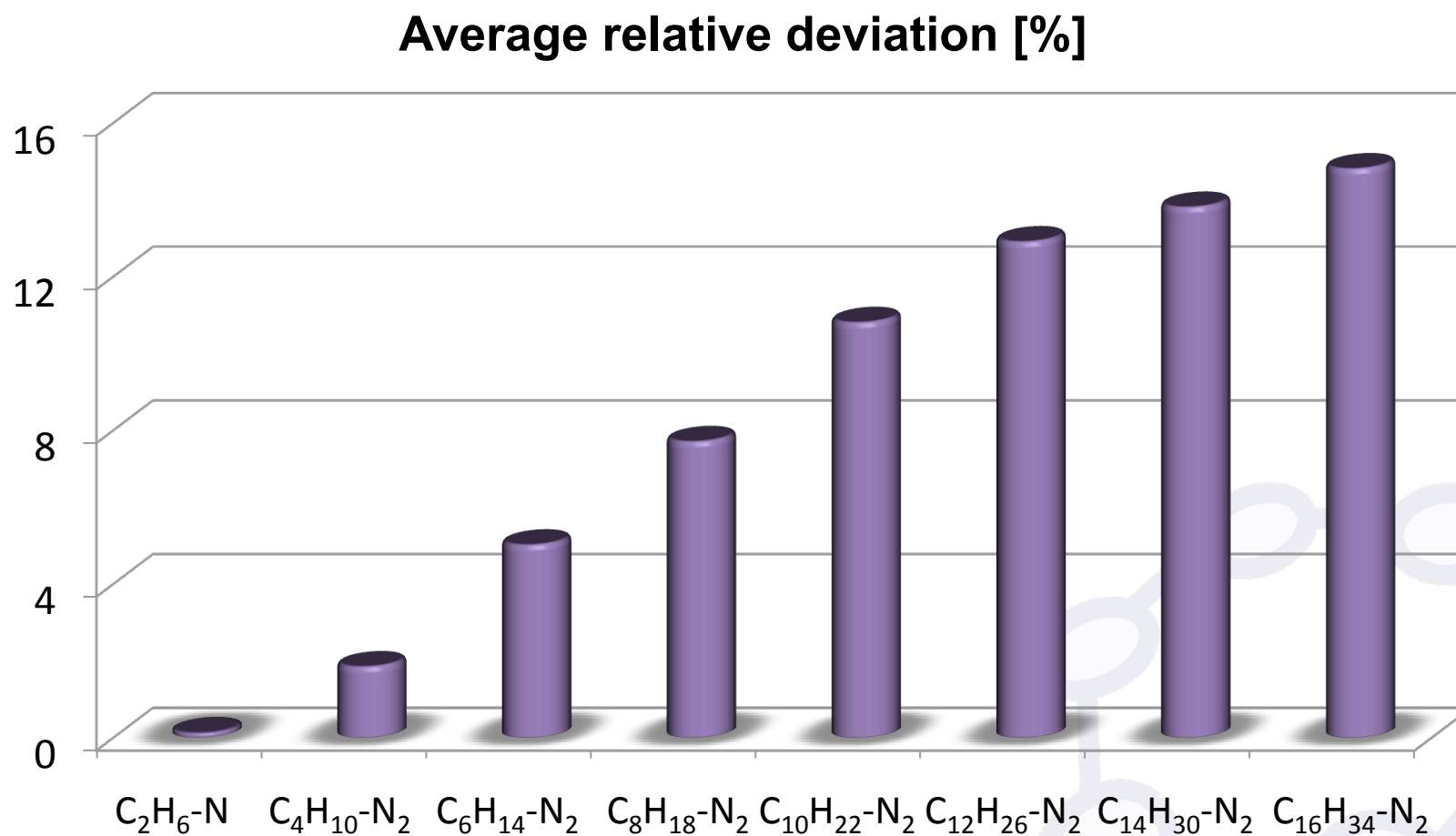
D. Gavril, J. Chromatography A,
1037, Vol. 147, 2004]

Target systems -1

N-alkanes/ N_2 mixtures (300 alkanes + 3000 N_2)

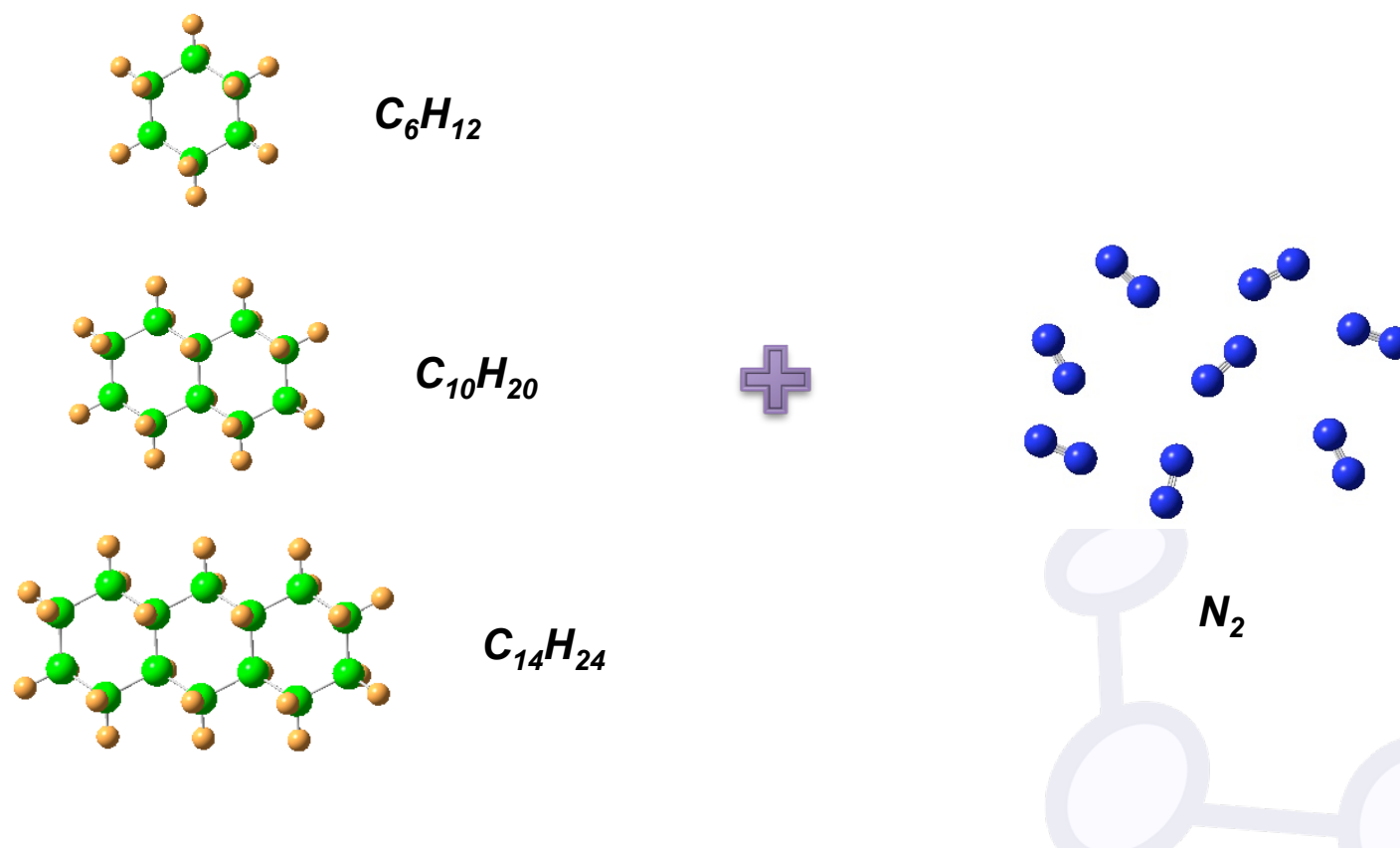


Comparison with C-E equation [n-alkanes]

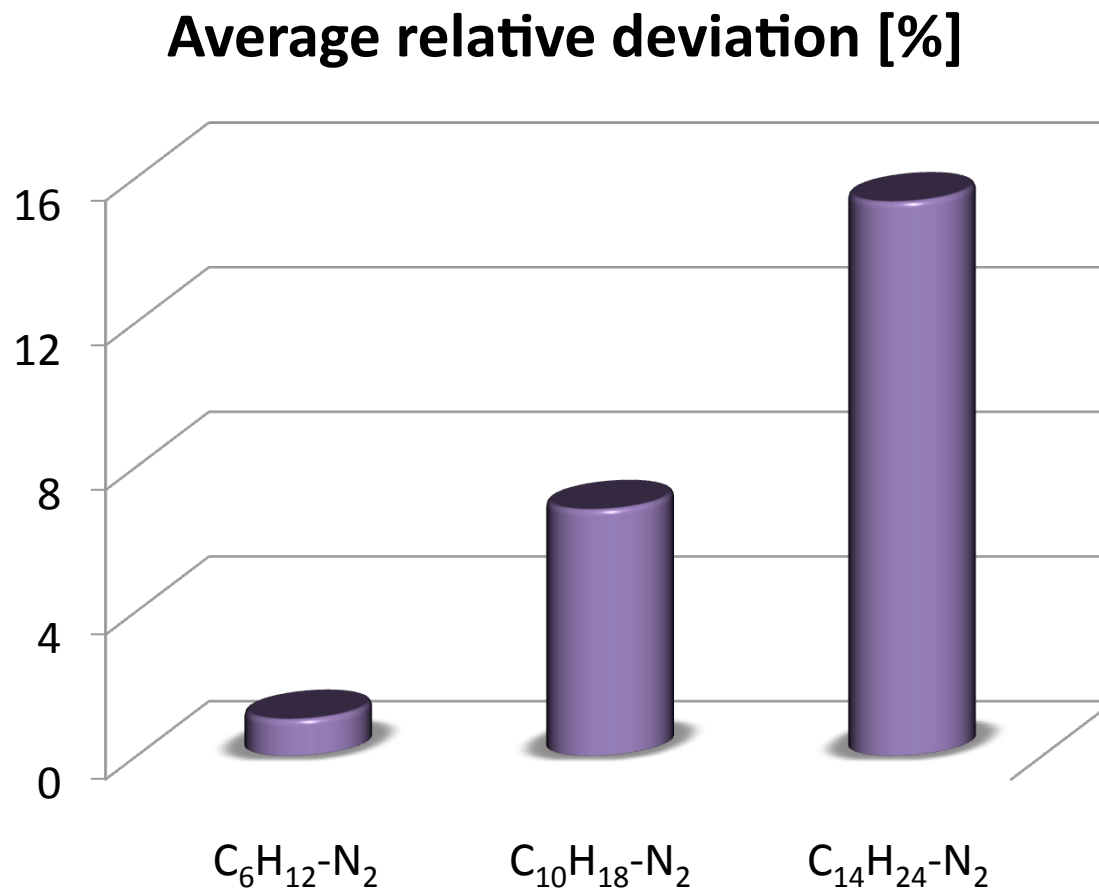


Target systems -2

Cycloalkanes/ N_2 mixtures (300 alkanes + 3000 N_2)



Comparison with C-E equation [cycloalkanes]



Milestones

- Transport properties of hydrocarbons using MD simulations (emphasis on compounds present in the JetSurF mechanism)
- N-alkanes and branched alkanes
- Work in progress for cycloalkanes
- New L-J parameters that can be used in combustion codes
- Tracer coefficients for multi-component diffusion coefficients

Conclusions

- ❑ We have implemented a tool to compute binary mass diffusivities for hydrocarbons using atomistic simulations.
- ❑ This computational tool can be used to quantify the effect of molecular structure on diffusivity
- ❑ The combination of updated kinetics and transport data for jet fuel surrogates will allow the development of a kinetic mechanism that can be used in many combustion conditions, **including flames**.